Densities of Aqueous Solutions of Sodium Bisulfite and Sodium 2-Methylallyl Sulfate

N. V. Choudary and R. V. Jasra*

Research Centre, Indian Petrochemicals Corporation Limited, Vadodara 391 346, India

Densities of aqueous solutions of sodium 2-methylallyl sulfate and sodium bisulfite have been measured at six temperatures in the range 283.15–303.15 K. The measured density values are represented by an empirical equation. The fitting of the experimental results for sodium 2-methylallyl sulfate is excellent, whereas in the case of sodium bisulfite the fitted data are in reasonably good agreement with the experimental values.

Introduction

In commercial processes acrylic fiber is manufactured by suspension polymerization with water as the suspension medium in the presence of a redox catalyst. In the catalyst preparation, aqueous solutions of sodium nitrite, potassium cyanate, sodium bisulfite, and sulfuric acid are used. In these processes, sodium 2-methylallyl sulfate is used as a comonomer to enhance the dyeability of the fiber. Catalyst batch preparation requires frequent monitoring of concentrations of aqueous solutions of these compounds. One of the simplest ways of obtaining the concentration of a solution is to measure the density of the solution. The density of aqueous solutions of sulfuric acid (1-3), sodium nitrite (1, 4), and potassium cyanate (1) are available in the published literature. However, no published literature values are available for densities of aqueous solutions of sodium 2-methylallyl sulfate and sodium bisulfite. In the present paper, we report densities of aqueous solutions of sodium 2-methylallyl sulfate and sodium bisulfite

as a function of concentration and temperature from 283.15 to 313.15 K.

Experimental Section

Densities are measured with an Anton Paar digital density meter, model DMA 602H. The density determination is based on measuring the time period of oscillation of a vibrating U-shaped glass sample tube which is filled with the sample liquid. The following relationship exists between the time period of vibration of the glass tube and the density of the solution filled in the vibrating tube:

$$\rho = A(t^2 - B) \tag{1}$$

where t is the time period and A and B are instrument constants which are determined by calibration with fluids of precisely known densities, viz., water and air. The density values obtained in the present study were accurate to ± 0.01 kg·m⁻³.

| Table 1. | Density, a. of Sodium 2-Met | hvlallvl Sulfate at 283.75. | . 288.15, 293.15, 298.15, 303.15, and 313.15 K |
|------------------|-------------------------------|---------------------------------|--|
| A WOLD 11 | 204010,, p, 01 2041414 2 1100 | = = = = = = = = = = = = = = = = | , =conc, =conc, =conc, coonc, and crone |

| | $ ho/(kg\cdot m^{-3})$ | | | $ ho/(kg\cdot m^{-3})$ | |
|-------------------------------------|-----------------------------|---------------------|-------------------------------------|-------------------------|---------------------|
| $c/(\text{mol}\cdot\text{kg}^{-1})$ | T = 283.75 K | T = 288.15 K | $c/(\text{mol}\cdot kg^{-1})$ | T = 283.75 K | T = 288.15 K |
| 0.0078 | 1000.172 | 999.617 | 0.9193 | 1054.374 | 1053,242 |
| 0.0345 | 1001.932 | 1001.362 | 0.9520 | 1056.170 | 1055.062 |
| 0.0643 | 1003.888 | 1003.427 | 0.9713 | 1057.185 | 1055.976 |
| 0.2983 | 1018.604 | 1017.922 | 1.0061 | 1058.977 | 1057.896 |
| 0.6331 | 1038.188 | 1037.401 | 1.1288 | 1065.663 | 1064.349 |
| 0.7528 | 1045.089 | 1044.169 | 1.2633 | 1072.791 | 1071.394 |
| 0.8803 | 1052.193 | 1051.151 | | | |
| | ρ/(kg·m ⁻³) | | | ρ/(kg·m ⁻³) | |
| $c/(\text{mol}\cdot\text{kg}^{-1})$ | T = 293.15 K | T = 298.15 K | $c/(\text{mol}\cdot kg^{-1})$ | T = 293.15 K | <i>T</i> = 298.15 K |
| 0.0065 | 998.658 | 997.453 | 0.8803 | 1049.569 | |
| 0.0302 | 1000.175 | 998.963 | 0.9163 | 1051.476 | 1049.497 |
| 0.0643 | 1002.347 | 1001.107 | 0.9538 | 1053.393 | 1051.427 |
| 0.2983 | 1016.809 | | 0.9787 | 1054.756 | 1052.698 |
| 0.3209 | | 1016.321 | 1.0080 | 1056.290 105 | |
| 0.6283 | 1035.851 | 1033.839 | 1.1331 | 1062.660 | 1060.988 |
| 0.7574 | 1042.964 | 1040.787 | 1.2902 | 1070.519 | 1069.135 |
| | ρ/(k | g•m ⁻³) | | ρ/(kg | g•m ^{−3}) |
| c/(mol·kg ⁻¹) | T = 303.15 K | T = 313.15 K | $c/(\text{mol}\cdot\text{kg}^{-1})$ | T = 303.15 K | T = 313.15 K |
| 0.0078 | 996.157 | 992.720 | 0.9193 | 1047.886 | 1043.809 |
| 0.0345 | 997.846 | 994.376 | 0.9520 | 1049.663 | 1045.493 |
| 0.0643 | 999.705 | 996.193 | 0.9713 | 1050.639 | 1046.431 |
| 0.2983 | 1013.750 | 1010.038 | 1.0061 | 1052.387 | 1048.278 |
| 0.6331 | 1032.618 | 1028.715 | 1.1288 | 1058.746 | 1054.541 |
| 0.7528 | 1039.141 | 1035.069 | 1.2633 | 1065.555 | 1061.205 |
| 0.8803 | 1045.874 | 1041.820 | | | |

| Table | 2. Der | ısity, ρ, o | f Sodium | Bisulfite | at 293.3 | 75, 288.15, |
|--------|-----------|-------------|-----------|-----------|----------|-------------|
| 293.15 | , 298.15, | 303.15, a | nd 313.15 | K | | |

| | $\rho/(\text{kg}\cdot\text{m}^{-3})$ | | | | |
|---|---|---|---|--|--|
| $c/(\text{mol}\cdot\text{kg}^{-1})$ | T = 283.15 K | T = 288.15 K | <i>T</i> = 293.15 K | | |
| 0.0099 | 1000.802 | 1000.129 | 999.154 | | |
| 0.0483 | 1003.981 | 1003.297 | 1002.144 | | |
| 0.0985 | 1008.214 | 1007.315 | 1006.269 | | |
| 0.1179 | 1009.338 | 1008.553 | 1007.493 | | |
| 0.4536 | 1034.275 | 1033.229 | 1032.164 | | |
| 0.8981 | 1068.218 | 1066.456 | 1064.980 | | |
| 1.3988 | 1105.329 | 1102.998 | 1099.893 | | |
| 1.9151 | 1136.683 | 1134.862 | 1132.093 | | |
| 2.1883 | 1152.982 | 1150.374 | 1147.724 | | |
| 2.4717 | 1168.626 | 1166.720 | 1164.472 | | |
| 2.5478 | 1173.825 | 1171.504 | 1168.685 | | |
| 2.6895 | 1182.093 | 1179.693 | 1177.580 | | |
| 2.7636 | 1186.924 | 1184.467 | 1182.070 | | |
| 2.8919 | 1195.432 | 1192.322 | 1190.227 | | |
| 2.9155 | 1196.573 | 1193.965 | 1191.757 | | |
| 3.0844 | 1209.897 | 1205.794 | 1203.555 | | |
| | | | | | |
| | | $ ho/({ m kg}{ m m}^{-3})$ | | | |
| c/(mol·kg ⁻¹) | <i>T</i> = 298.15 K | $\rho/(\text{kg-m}^{-3})$ T = 303.15 K | <i>T</i> = 313.15 K | | |
| c/(mol·kg ⁻¹) | T = 298.15 K 997.818 | $\rho/(\text{kg}\cdot\text{m}^{-3})$ T = 303.15 K 996.786 | T = 313.15 K 993.307 | | |
| c/(mol·kg ⁻¹) 0.0099 0.0483 | T = 298.15 K 997.818 1000.867 | $\frac{\rho/(\text{kg}\cdot\text{m}^{-3})}{T = 303.15 \text{ K}}$ 996.786 998.143 | <i>T</i> = 313.15 K 993.307 996.402 | | |
| c/(mol·kg ⁻¹) 0.0099 0.0483 0.0985 | T = 298.15 K 997.818 1000.867 1004.655 | $\frac{\rho/(\text{kg-m}^{-3})}{T = 303.15 \text{ K}}$ 996.786 998.143 1003.617 | <i>T</i> = 313.15 K 993.307 996.402 | | |
| c/(mol·kg ⁻¹) 0.0099 0.0483 0.0985 0.1179 | T = 298.15 K 997.818 1000.867 1004.655 1006.084 | $\rho/(\text{kg-m}^{-3})$ $T = 303.15 \text{ K}$ 996.786 998.143 1003.617 1004.903 | <i>T</i> = 313.15 K 993.307 996.402 1003.564 | | |
| c/(mol·kg ⁻¹) 0.0099 0.0483 0.0985 0.1179 0.4536 | T = 298.15 K 997.818 1000.867 1004.655 1006.084 1031.084 | $\frac{\rho/(\text{kg}\cdot\text{m}^{-3})}{T = 303.15 \text{ K}}$ 996.786 998.143 1003.617 1004.903 1031.483 | T = 313.15 K 993.307 996.402 1003.564 1028.076 | | |
| c/(mol·kg ⁻¹) 0.0099 0.0483 0.0985 0.1179 0.4536 0.8981 | T = 298.15 K 997.818 1000.867 1004.655 1006.084 1031.084 1062.635 | $\frac{\rho/(\text{kg}\cdot\text{m}^{-3})}{T = 303.15 \text{ K}}$ 996.786 998.143 1003.617 1004.903 1031.483 1063.736 | T = 313.15 K 993.307 996.402 1003.564 1028.076 1059.745 | | |
| c/(mol·kg ⁻¹) 0.0099 0.0483 0.0985 0.1179 0.4536 0.8981 1.3988 | T = 298.15 K 997.818 1000.867 1004.655 1006.084 1031.084 1062.635 1096.236 | $\rho/(\text{kg·m}^{-3})$ $T = 303.15 \text{ K}$ 996.786 998.143 1003.617 1004.903 1031.483 1063.736 | T = 313.15 K 993.307 996.402 1003.564 1028.076 1059.745 | | |
| c/(mol·kg ⁻¹) 0.0099 0.0483 0.0985 0.1179 0.4536 0.8981 1.3988 1.9151 | T = 298.15 K 997.818 1000.867 1004.655 1006.084 1031.084 1062.635 1096.236 1129.815 | $\rho/(\text{kg·m}^{-3})$ $T = 303.15 \text{ K}$ 996.786 998.143 1003.617 1004.903 1031.483 1063.736 1127.921 | T = 313.15 K 993.307 996.402 1003.564 1028.076 1059.745 1123.935 | | |
| c/(mol·kg ⁻¹) 0.0099 0.0483 0.0985 0.1179 0.4536 0.8981 1.3988 1.9151 2.1883 | T = 298.15 K 997.818 1000.867 1004.655 1006.084 1031.084 1062.635 1096.236 1129.815 1145.639 | $\rho/(\text{kg}\cdot\text{m}^{-3})$ $T = 303.15 \text{ K}$ 996.786 998.143 1003.617 1004.903 1031.483 1063.736 1127.921 1143.596 | T = 313.15 K 993.307 996.402 1003.564 1028.076 1059.745 1123.935 | | |
| c/(mol·kg ⁻¹) 0.0099 0.0483 0.0985 0.1179 0.4536 0.8981 1.3988 1.9151 2.1883 2.4717 | T = 298.15 K 997.818 1000.867 1004.655 1006.084 1031.084 1062.635 1096.236 1129.815 1145.639 1163.119 | $\rho/(\text{kg-m}^{-3})$ $T = 303.15 \text{ K}$ 996.786 998.143 1003.617 1004.903 1031.483 1063.736 1127.921 1143.596 1159.090 | T = 313.15 K 993.307 996.402 1003.564 1028.076 1059.745 1123.935 1153.810 | | |
| c/(mol·kg ⁻¹) 0.0099 0.0483 0.0985 0.1179 0.4536 0.8981 1.3988 1.9151 2.1883 2.4717 2.5478 | T = 298.15 K 997.818 1000.867 1004.655 1006.084 1031.084 1062.635 1096.236 1129.815 1145.639 1163.119 1167.487 | $\rho/(\text{kg-m}^{-3})$ $T = 303.15 \text{ K}$ 996.786 998.143 1003.617 1004.903 1031.483 1063.736 1127.921 1143.596 1159.090 1163.112 | T = 313.15 K 993.307 996.402 1003.564 1028.076 1059.745 1123.935 1153.810 1157.427 | | |
| c/(mol·kg ⁻¹) 0.0099 0.0483 0.0985 0.1179 0.4536 0.8981 1.3988 1.9151 2.1883 2.4717 2.5478 2.6895 | T = 298.15 K 997.818 1000.867 1004.655 1006.084 1031.084 1062.635 1096.236 1129.815 1145.639 1163.119 1167.487 1175.799 | $\rho/(\text{kg-m}^{-3})$ $T = 303.15 \text{ K}$ 996.786 998.143 1003.617 1004.903 1031.483 1063.736 1127.921 1143.596 1159.090 1163.112 1171.112 | T = 313.15 K 993.307 996.402 1003.564 1028.076 1059.745 1123.935 1153.810 1157.427 1164.676 | | |
| c/(mol·kg ⁻¹) 0.0099 0.0483 0.0985 0.1179 0.4536 0.8981 1.3988 1.9151 2.1883 2.4717 2.5478 2.6895 2.7636 | $\overline{T} = 298.15 \text{ K}$ 997.818 1000.867 1004.655 1006.084 1031.084 1062.635 1096.236 1129.815 1145.639 1163.119 1167.487 1175.799 1179.925 | $\begin{array}{c} \rho/(\mathrm{kg}\cdot\mathrm{m}^{-3})\\ \hline T=303.15~\mathrm{K}\\ 996.786\\ 998.143\\ 1003.617\\ 1004.903\\ 1031.483\\ 1063.736\\ \hline 1127.921\\ 1143.596\\ 1159.090\\ 1163.112\\ 1171.112\\ 1175.313\\ \end{array}$ | T = 313.15 K 993.307 996.402 1003.564 1028.076 1059.745 1123.935 1153.810 1157.427 1164.676 1167.278 | | |
| c/(mol·kg ⁻¹) 0.0099 0.0483 0.0985 0.1179 0.4536 0.8981 1.3988 1.9151 2.1883 2.4717 2.5478 2.6895 2.7636 2.8919 | T = 298.15 K 997.818 1000.867 1004.655 1006.084 1031.084 1062.635 1096.236 1129.815 1145.639 1163.119 1167.487 1175.799 1179.925 1187.104 | $\begin{array}{c} \rho/(\text{kg-m}^{-3})\\ \hline T=303.15 \text{ K}\\ 996.786\\ 998.143\\ 1003.617\\ 1004.903\\ 1031.483\\ 1063.736\\ \hline 1127.921\\ 1143.596\\ 1159.090\\ 1163.112\\ 1171.112\\ 1175.313\\ 1181.469\\ \hline \end{array}$ | T = 313.15 K 993.307 996.402 1003.564 1028.076 1059.745 1123.935 1153.810 1157.427 1164.676 1167.278 1172.282 | | |
| c/(mol·kg ⁻¹) 0.0099 0.0483 0.0985 0.1179 0.4536 0.8981 1.3988 1.9151 2.1883 2.4717 2.5478 2.6895 2.7636 2.8919 2.9155 | T = 298.15 K 997.818 1000.867 1004.655 1006.084 1031.084 1062.635 1096.236 1129.815 1145.639 1163.119 1167.487 1175.799 1179.925 1187.104 1188.344 | $\rho/(\text{kg·m}^{-3})$ $T = 303.15 \text{ K}$ 996.786 998.143 1003.617 1004.903 1031.483 1063.736 1127.921 1143.596 1159.090 1163.112 1171.112 1175.313 1181.469 1182.547 | T = 313.15 K 993.307 996.402 1003.564 1028.076 1059.745 1123.935 1153.810 1157.427 1164.676 1167.278 1172.282 1173.601 | | |

Table 3. Standard Deviation σ (ρ) and Values of Constants in Equation 2 for Sodium 2-Methylalyl Sulfate at Various Temperatures

| T/K | A_2 | A_3 | A_4 | A_5 | A_6 | $\sigma(ho)/({\rm kg}\cdot{\rm m}^{-3})$ |
|--------|--------|---------|---------|--------|---------|---|
| 283.75 | 68.341 | -9.012 | -0.237 | | | 0.05 |
| 288.15 | 65.034 | 20.083 | -75.372 | 74.062 | -25.299 | 0.07 |
| 293.15 | 68.537 | -10.953 | | | | 0.06 |
| 298.15 | 64.355 | -7.468 | | | | 0.06 |
| 303.15 | 66.063 | -10.560 | 0.984 | | | 0.03 |
| 313.15 | 64.418 | -8.663 | | | | 0.04 |

The temperature of the measuring cell was maintained within ± 0.001 K with the help of a circulating thermostat whose temperature was controlled by an M/S TRONIC precision temperature controller, model PTC-41.

Sodium 2-methylallyl sulfate and sodium bisulfate were Analar grade and were used without further purification. Sodium 2-methylallyl sulfate contained 200 ppm each Cland sodium sulfite as impurities. On the other hand sodium bisulfite contained 10 ppm Cl- and 15 ppm Fe³⁺ as impurities. Aqueous solutions of various known concentrations were prepared by mass using triple-distilled water. Solutions of low concentrations were prepared by successive dilutions.



Figure 1. Deviation of the estimated density (from eq 2) from the experimental density plotted as a function of the square root of concentration for sodium 2-methylallyl sulfate.



Figure 2. Deviation of the estimated density (from eq 2) from the experimental density plotted as a function of the square root of concentration for sodium bisulfite.

Results and Discussion

Experimental density values for sodium 2-methylallyl sulfate and sodium bisulfite measured at 283.15, 288.15, 293.15, 298.15, 303.15, and 313.15 K are given in Tables 1 and 2. The values of density may be expressed by an empirical equation of the form given below:

$$\rho_T / (\text{kg·m}^{-3}) = \rho_W / (\text{kg·m}^{-3}) + \sum_{i=2}^n A_i (c/(\text{mol·kg}^{-1}))^{i/2} \quad (2)$$

where ρ_T is the density of the solution at temperature T, ρ_W is the density of water, c is the concentration of the solution (mol·kg⁻¹), and A_i are adjustable parameters. The values of adjustable parameters obtained by least-squares regression along with the standard deviation $\sigma(\rho)$ calculated using eq 3,

$$\sigma(\rho) = \left[\frac{\left(\rho_{\text{calcd}} - \rho_{\text{exptl}}\right)^2}{(n-p)}\right]^{1/2}$$
(3)

where n is the number of data and p is the number of adjustable parameters, are given in Tables 3 and 4. The

Table 4. Standard Deviation $\sigma(\rho)$ and Vlaues of Constants in Equation 2 for Sodium Bisulfite at Various Temperatures

| T/K | A_2 | A ₃ | A ₄ | A_5 | A_6 | A ₇ | $\sigma(ho)/({ m kg}\cdot{ m m}^{-3})$ |
|--------|-------|----------------|----------------|----------|----------|----------------|---|
| 283.15 | 1.226 | 111.890 | -170.777 | 276.037 | -184.613 | 42.463 | 0.324 |
| 288.15 | 0.560 | 111.739 | -167.838 | 267.297 | -176.678 | 40.188 | 0.248 |
| 293.15 | 0.454 | 99.581 | -112.779 | 182.207 | -124.243 | 28.990 | 0.147 |
| 298.15 | 0.155 | 78.125 | -3.359 | -2.342 | | | 0.206 |
| 303.15 | 7.910 | 22.761 | 147.078 | -167.222 | 78.415 | -13.787 | 0.169 |
| 313.15 | 5.524 | 46.510 | 93.865 | -125.931 | 69.373 | -14.818 | 0.352 |

deviation of the estimated density from the experimental density for both the components is plotted in Figures 1 and 2. As can be seen from these figures the fitting is excellent in the case of sodium 2-methylallyl sulfate. The deviation was less than ± 0.1 kg·m⁻³. However, in the case of sodium bisulfite the deviation for most of the data points was within ± 0.2 kg·m⁻³ with a maximum deviation of ± 0.53 kg·m⁻³

Acknowledgment

We acknowledge the experimental assistance of Mr. R. D. Parte. We are thankful to Dr. S. G. T. Bhat for his keen interest and useful discussions and Dr. I.S. Bhardwaj, Director (R&D), for his encouragement. We are also thankful to Indian Petrochemicals Corp. Ltd., Vadodara, for permission to publish this work.

Literature Cited

- (1) International critical tables; McGraw-Hill: New York, 1928; Vol. III.
- (2)
- (3)
- III.
 D'Ans/Lax. Taschenbuch fur chemiker und physiker; Springer: Berlin, 1967; Band I.
 Donke, J.; Bein, W. Z. Z. Anorg. Chem. 1905, 43, 125.
 Timmermann, J. Physico-chemical constants of binary systems in concentrated solutions; Interscience: New York, 1960; Vols. 3 and (4) 4.

Received for review October 1, 1993. Accepted October 25, 1993.

• Abstract published in Advance ACS Abstracts, December 1, 1993.